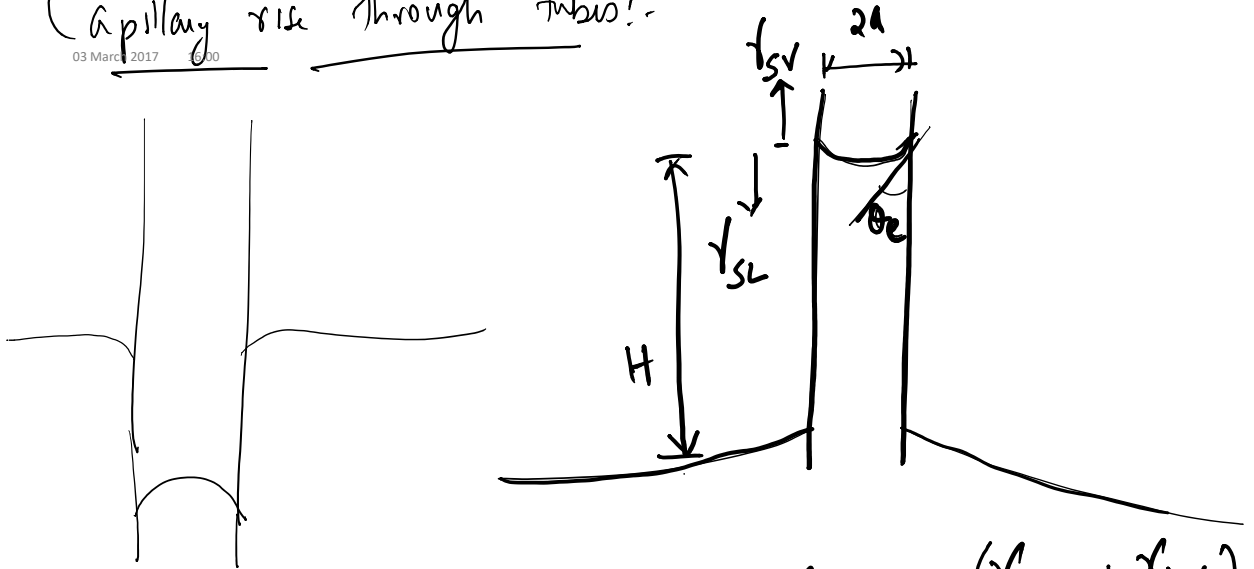


Capillary rise through tubes:-



Spreading parameter: $S = \gamma_{sv} - (\gamma_{sl} + \gamma_{lv})$

We can also define a new parameter:

$$I = \gamma_{sv} - \gamma_{sl} = \frac{\gamma_{lv}}{\sigma} \cos \theta_c$$

$I > 0$, if $\theta_c < 90^\circ$, else $I < 0$

We said, $S > 0 \Rightarrow$ Complete spreading.

I : Impregnation parameter.

It is much easier to obtain $I > 0$

than $S > 0 \Rightarrow$ In nature we usually encounter partial spreading.

Total energy of the system:- \rightarrow Water column

Total energy of the system:-

$$E = (\gamma_{SL} - \gamma_{SV}) 2\pi a H + \int g \pi a^2 \frac{H^2}{2}$$

$$= \underbrace{-I \cdot 2\pi a H}_{\text{Surface energy}} + \underbrace{\int g \pi a^2 \frac{H^2}{2}}_{\text{gravitational P.E}}$$

Height chosen can be obtained by minimizing energy:-

$$\frac{\partial E}{\partial H} = 0 \Rightarrow -2\pi a \cdot I + \int g \pi a^2 H = 0$$

$$\Rightarrow H = \frac{2\pi a I}{\int g \pi a^2} = \frac{2I}{\int g a}$$

But $I = \sigma \cos \theta$

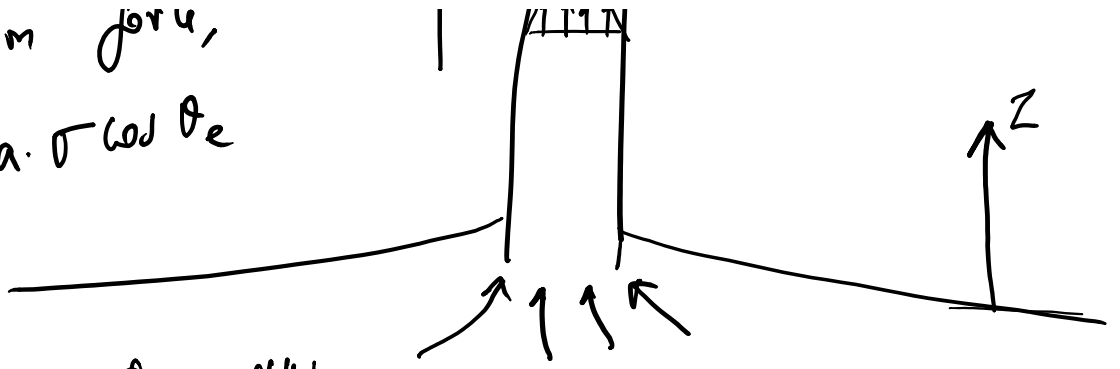
$$\Rightarrow \boxed{H = \frac{2\sigma \cos \theta}{\int g a}} \quad \therefore \text{Jurin's Law}$$

Dynamics of Impregnation:-

force causing the fluid to rise is surface tension force,



Surface tension force,
 $F = 2\pi a \cdot \sigma \cos \theta_e$



forces opposing this rise:-

- Gravity
- Viscosity
- Inertia

$$\frac{d}{dt}(Mv) = F - F_m - \underbrace{W}_{\text{weight}} = Mg$$

F_m : Assuming the flow is fully developed, (this happens only after a viscous time, $t_v = \frac{a^2}{\nu}$),

$$u(r) = 2\dot{z} \left(1 - \frac{r^2}{a^2}\right)$$

$\dot{z} = V$: average velocity

Shear stress : $\tau = \mu \left. \frac{\partial u}{\partial r} \right|_{r=a} = -\frac{4\mu}{a} \dot{z}$

$$= -\frac{4\mu}{a} \cdot V$$

$$F_m = 2\pi a \cdot z \cdot \frac{-4\mu}{a} \cdot V$$

$$= -8\pi \mu V z$$

$$\frac{d}{dt}(Mv) = \underbrace{2\pi a \cdot \gamma \cos\theta}_F - \underbrace{8\pi\mu Vz}_{F_\mu} - \underbrace{Mg}_W$$

Viscous regime:- Valid for times $> t_v$

Ignoring inertia since the fluid rises slowly at later times, we get

$$F - F_\mu - W = 0$$

$$\Rightarrow F - W = F_\mu$$

For thin capillary tubes, $F \propto$ Surface area
 $W \propto$ Volume

$$\Rightarrow F \gg W$$

$$\Rightarrow F \approx F_\mu$$

$$\begin{aligned} \Rightarrow 2\pi a \cdot \sigma \cos\theta_e &= 8\pi\mu Vz \\ &= 8\pi\mu z \cdot \dot{z} \\ &= 8\pi\mu \frac{d}{dt} \left(\frac{z^2}{2} \right) \end{aligned}$$

$$\Rightarrow \frac{d}{dt} \left(\frac{z^2}{2} \right) = \frac{2\pi a \sigma \cos\theta_e}{8\pi\mu}$$

$$\frac{d}{dt}(z^2) = \frac{1}{2} \frac{a \sigma \omega \theta e}{\mu}$$

Integration:- $z^2 \approx \frac{1}{2} \frac{a \sigma \omega \theta e}{\mu} \cdot t$

or $z \sim \left(\frac{1}{2} \frac{\sigma a \omega \theta e}{\mu} \right)^{1/2} \cdot \sqrt{t}$

↳ Washburn Law/formula

Inertial regime:-

This is valid at short times, i.e.;

$$t \ll \tau_y$$

Also at short times, W can be ignored.

$$\frac{d}{dt}(Mv) = F \quad \left(\begin{array}{l} \text{Ignoring viscosity} \\ \text{forces} \end{array} \right)$$

$$\frac{d}{dt} \left(\cancel{\rho \cdot \pi a^2} z(t) \cdot \dot{z} \right) = \cancel{2\pi a} \cdot \sigma \omega \theta e$$

$$\frac{d}{dt} (z \cdot \dot{z}) = \frac{2\sigma \omega \theta e}{\rho a}$$

$$\text{or } \frac{d}{dt} (z \dot{z}) \sim \frac{2\sigma \omega \theta e}{\rho a}$$

|
dz
dt

$$\frac{d^2}{dt^2} \left(\frac{z^2}{2} \right) \sim \frac{2\sigma \omega \theta e}{\rho a}$$

$$z \cdot \dot{z} = \frac{2\sigma \omega \theta e}{\rho a} \cdot t$$

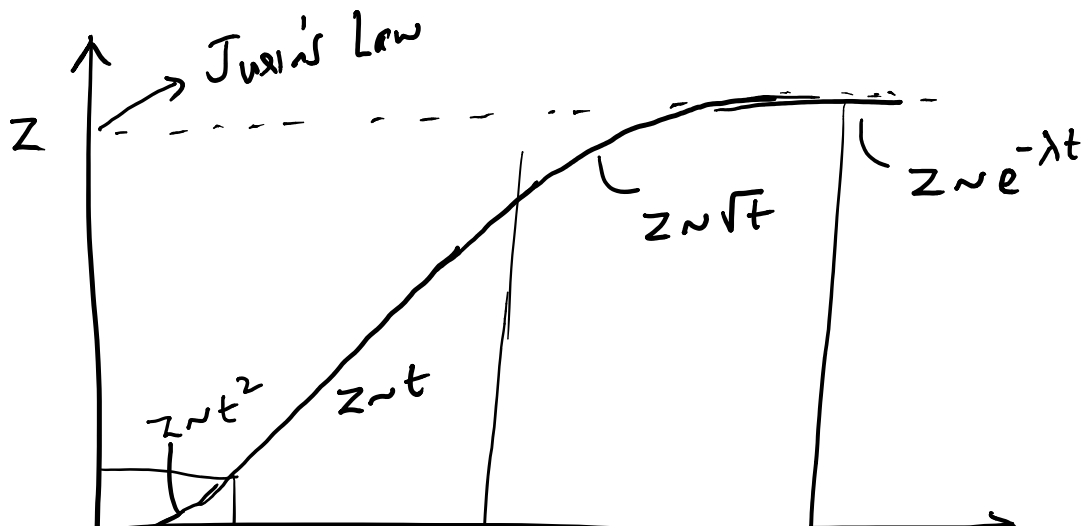
$$\frac{d}{dt} \left(\frac{z^2}{2} \right) = \frac{2\sigma \omega \theta e}{\rho a} \cdot t$$

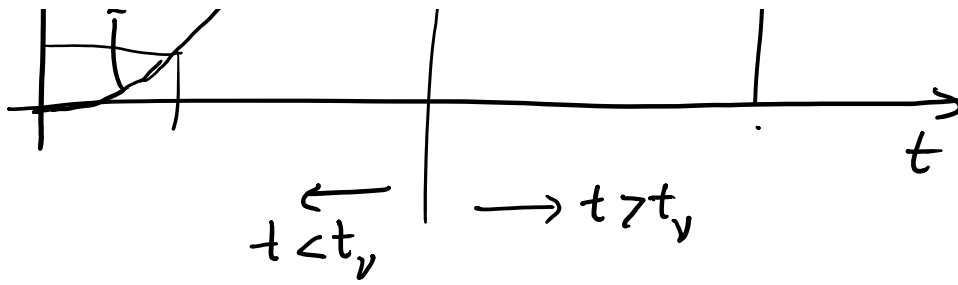
$$d \left(\frac{z^2}{2} \right) = \frac{2\sigma \omega \theta e}{\rho a} \cdot t \, dt$$

$$\frac{z^2}{2} = \frac{2\sigma \omega \theta e}{\rho a} \cdot \frac{t^2}{2}$$

$$\Rightarrow z^2 = \frac{2\sigma \omega \theta e}{\rho a} \cdot t^2$$

$$\Rightarrow z(t) = \left(\frac{2\sigma \omega \theta e}{\rho a} \right)^{1/2} \cdot t$$





$$\delta \sim \sqrt{\nu t} \sim \sqrt{\nu t_v} \sim \sqrt{\nu \frac{a^2}{\nu}} = a$$